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Toward high production of graphene flakes – a review on recent developments in their synthesis methods and scalability

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Research and development in graphene synthesis has been rapidly growing in the past few years because of its extraordinary physical, mechanical, thermal, electrical and optical properties. Graphene flakes, one of the most popular forms of graphene, can be used for many applications such as conductive inks, nanofluids, supercapacitors, composites, etc. Synthesis of graphene flakes is indeed a path to reach large-scale production even if the cost of production and efficiency are required to be further improved. This review sheds light on the recent advancements of graphene flake synthesis and it gives a comprehensive analysis of the synthesis methods. Keys for further improvements are proposed based on the mechanisms involved in the graphene flake formation.

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1 Introduction

The introduction of new materials has enabled the growth of new technologies that have a beneficial impact on society. Currently, we are on the verge of a new age of 2-dimensional (2D) materials. Boron nitride (BN),1-3 bismuth telluride (Bi₂Te₃),^{4,5} bismuth(III) selenide (Bi₂Se₃),⁶ molybdenum disulfide (MoS₂),^{7,8} molybdenum diselenide (MoSe₂),^{9,10} molybdenum ditelluride (MoTe₂),¹¹ tungsten disulfide (WS₂),¹² tungsten diselenide (WSe2),13,14 silicone,15,16 phosphorene,17,18 bismuthene,19 graphyne,20,21 graphane22 and graphene23,24 are among the 2D materials that have been investigated. Within this group, graphene has been the most-researched material since its discovery in 2004.25,26 It is investigated for use in next generation devices due to its outstanding combination of properties not observed in any other type of material. Its magnificent properties are attributed to the strong bonding between the hexagonal arrangements of carbon atoms that make up graphene.

Graphene can be produced in several forms including flakes,^{27–29} ribbons,^{30,31} and large-area sheets.^{32,33} They differ in

lateral dimensions; flakes with limited lateral dimension (from several nanometers to micrometers), large-area sheets possessing macroscopic and extended lateral dimensions, while ribbons have one lateral dimension that is at least one order of magnitude larger than the others.34 These differences allow graphene to be used in various types of applications. For example, large-area graphene sheets are more suited for waferscale thin film-like applications such as transparent conductive electrodes,35 while graphene flakes (GFs) are investigated for conductive ink applications.36,37 This review focuses on the various synthesis methods of GFs. This form of graphene is also sometimes referred to as graphene nanosheets,38-44 graphene microsheets,45 graphene platelets (or nanoplatelets),46,47 graphene powder48,49 or graphene quantum dots50,51 by other researchers. Until today, reviews on GFs have been mainly limited to chemical methods such as pre-oxidization via Hummers' method or modified Hummers' method before exfoliation. However, it is often ignored that several developed physical methods are able to produce large volumes of GFs of good quality that would be suitable for applications that demand greater quality than that produced by chemical methods. Indeed, graphene oxide (GO) and reduced graphene oxide (rGO) produced by these chemical methods contain many defects and they can be considered as a different class of graphene materials with their own advantages. In this review paper, GF syntheses from graphite by these alternative methods including ball-milling, sonication, shock waves, shearing in liquid and electrochemical methods are analyzed and discussed. The review is organized in three main parts. The first part deals with compilation of the various methods of GF synthesis along with the basic mechanisms of the processes. The second part analyzes the advantages, disadvantages and

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potential of these synthesis methods for scaling-up. Lastly, some future prospects of the covered methods are given.

Synthesis of graphene flakes 2

Currently, exfoliation of graphite into GF synthesis mostly involves chemical oxidation of graphite to graphite oxide, followed by exfoliation to GO and then reduction to rGO in the presence of chemical reductants such as octadecyl amine,52 phenyl isocyanates,53 hydrazine,54 polymers55 and pyrene derivatives.56 GO and rGO are easily dispersed in various solvents which is beneficial for their processing for diverse applications such as in the formulation of water-based nanofluids for heat transfer usage,57 while GFs are difficult to disperse due to their hydrophobicity. Graphite oxide can be prepared by using Brodie's method,58 Hummers' method59 or a modified Hummers' method; 60 the latter two methods are the most prevalent. These techniques are, however, harmful since they involve the oxidative treatment of graphite with potassium permanganate (KMnO₄) and sodium nitrate (NaNO₃) in concentrated H₂SO₄. Such mixtures and other related procedures would generate toxic gases in the form of nitrogen dioxide (NO2) or dinitrogen tetroxide (N2O4).

Unlike graphene, rGO, prepared by reduction of GO, does not have the perfect graphene structure defined by the International Union of Pure and Applied Chemistry (IUPAC), which describes graphene as a "single carbon layer of graphite structure, describing its nature by analogy with a polycyclic aromatic hydrocarbon of quasi-infinite size".61 Bianco et al.34 recommended this rGO nomenclature to be "graphene oxide that has been reductively processed by chemical, thermal, microwave, photo-chemical, photo-thermal or microbial/bacteria methods to reduce its oxygen content". Even after a comprehensive reduction process, it is practically impossible to remove all of the oxygen functional groups on the rGO surface. This puts it in a different class than that of graphene⁶² and explains the reason why the term rGO is used instead of graphene. The presence of oxygen functional groups is responsible for its hydrophilic behavior but it would also disrupt the electronic properties of rGO, dramatically reducing its physical properties. The Raman D/G intensity ratio (I_D/I_G) is usually used to measure the extent of defects in the graphene structure. The $I_{\rm D}/I_{\rm G}$ of GO and rGO normally gives a high value between 1.0 and 2.0.38,63-65 Even so, it has been proven that GO and rGO were found to be very useful in catalysis and composites.66 However, other applications especially when high performance is required, such as in energy storage and generation devices⁶⁷ would demand a higher structural quality of graphene.

This review is focused on top-down methods, which have greater potential for production scale-up as opposed to the bottom-up chemical vapor deposition (CVD) technique. Previous reports show that the CVD methods were successfully utilized to synthesize GFs⁶⁸⁻⁷¹ using metal catalysts in the form of particles. CVD requires the use of expensive transition metal catalysts with comprehensive experimental setups that often involve flammable gases such as methane and acetylene. In order to grow graphene, heating at significantly high

temperatures ranging from 600 to 1000 °C is required and it often involves slow ramping and cooling processes. Since the metal catalyst has to be removed via a dissolution-filtrationdrying process before incorporation of graphene into applications, 72 it makes the whole process more costly, complicated and time-consuming. Nevertheless, CVD can produce better structural quality of graphene compared to its top-down counterpart, and its properties were found to be close to the pristine structure of graphene.39,73,74 Most large area graphene sheets were synthesized via CVD because of the demand for very high structural quality for their application. 32,75,76 However, the quantity and production cost take precedence for GF applications, which CVD cannot provide. In contrast to CVD, the topdown method offers lower cost but at the expense of quality, though still superior than GO and rGO. The next few parts will shine some light on the reported alternative techniques for large-scale GF synthesis.

2.1 Ball milling

Ball milling is a common method in the powder production industry known for its high production capacity and shear crushing force which is very well suited for the exfoliation of graphite to produce GFs. The ball milling technique involves breaking down graphitic microstructures into GFs via impact and attrition of metal balls striking the graphitic microstructures in a rotating hollow cylindrical shell. The rotation of the cylindrical shells creates a centrifugal force that will carry the grinding media such as zirconia balls in a turbulent and random manner so that the impact can transpire with greater effect. It works on the principle of particle size reduction in line with the top down route for GF synthesis. Generally, milling of graphite can be implemented in either a dry or a wet state. Dry milling can achieve a high yield of single layer GF but the use of an argon glove box is a downside, which makes the process more complicated. The average size of the GFs being produced depends heavily on the milling parameters, which include ballto-graphite ratio, initial weight of graphite, milling duration and milling revolution per minute (rpm). Table 1 shows, in detail, some examples of GF synthesis conditions via dry milling and the characteristics of the produced GFs.

In dry milling, milling agents are normally added alongside metal balls to reduce the stress induced in the graphitic structures.77,78 Alinejad and Mahmoodi79 used NaCl salt as a miller alongside zirconia balls with the ball-mill operated at 350 rpm for 2 hours under 0.4 MPa of argon atmosphere. The addition of NaCl particles which are substantially brittle and harder than graphite permits graphene nanoflakes of about $50 \times 200 \text{ nm}^2$ to be attained. The salt particles assist the shear stress mechanism of the zirconia balls and prevent GFs from agglomeration. Furthermore, they can be washed away easily with water after the milling process. In another study, Lv et al. 49 used Na₂SO₄ salt to produce graphene nanosheets in the size range of hundreds of square nanometers with ripple-like corrugations as shown in Fig. 1. Through mechanical peeling and post-milling washing, GFs were harvested at a low cost and have the potential to be scaled-up. The authors also claimed that the number of layers in

Table 1 Examples of GF synthesis via dry milling and their characteristics

Dry milling conditions					
Setup	Milling agent	Speed, duration, environment	Characteristics of produced graphene	Remarks	References
Planetary ball-mill, zirconia ball	NaCl	350 rpm, 2 hours, 0.4 MPa of Ar	Multilayer GF, size = $50 \times 200 \text{ nm}^2$	Use NaCl as a miller which could be washed away easily after milling	79
	Melamine (Na_2SO_4)	100 rpm, 30 min, air	$I_{\rm G}/I_{\rm D}=\sim$ 2.4, $L_{\rm a}=\sim$ 40 nm	Melamine disappeared upon washing with hot water	80
Stainless steel jar mill	Melamine	150 rpm, 24 hours	Graphene nanosheets with size in the range of hundreds of square nanometers, $I_{\rm D}/I_{\rm G}=0.507$ (for 200 : 1 of miller to graphite weight ratio)	Use Na ₂ SO ₄ as a miller which can be washed away easily after milling. XPS showed that GFs were not deeply oxidized during ball-milling	49
Planetary mill	Ammonia borane (NH ₃ BH ₃)	150 rpm, 4 hours	Single or few-layer GF, $<$ 6 layers, $I_D/I_G < 0.5$	Ammonia borane could be removed using ethanol	81
Planetary ball-mill, stainless steel ball	Milling agent = dry ice (KOH)	500 rpm, 48 hours	Edge carboxylated graphite, $I_{ m D}/I_{ m G}=1.16$	End product was graphite, purification required Soxhlet extraction with 1 M HCl to completely acidify carboxylates and to remove metallic impurities	40

the produced GFs can be controlled from two to tens of layers by merely changing the graphite to Na₂SO₄ ratio. In other studies, melamine (2,4,6-triamine-1,3,5-triazine)⁸⁰ and ammonia borane (NH₃BH₃)⁸¹ were investigated for their role in a dry ball-milling process. Herein, melamine and NH3BH3 did not act as millers but instead were used to weaken the van der Waals bonding between the graphite layers, which promotes easy exfoliation of graphite to produce GFs during the milling process.

It has been demonstrated in the past that stress reduction in graphitic materials can be achieved by wet milling. Table 2 lists some of the examples of GF synthesis via wet milling. Knieke et al.82 and Yao et al.41 successfully produced GFs from graphite powder in a wet milling process, i.e. in an anionic surfactant, sodium dodecyl sulfate (SDS). However, the drawback of using SDS is that it can adsorb on the surface of GF and is hard to remove. This is the reason why other solvents such as N,Ndimethylformamide (DMF),83 naphthol polyoxyethylene ether

(NPE),84 oxalic acid (C2H2O4)85 and 1-pyrenecarboxylic acid (1-PCA)⁸⁶ were also considered. Deng et al.⁸⁷ prepared surfactant-free few layer GFs by wet ball milling of graphite in N-methylpyrrolidone (NMP). GF production enhancement was observed according to the power law, but it was only achieved after continuous milling for 10 hours.

Kim et al.88 used wet-milling via a planetary ball-mill to produce GFs which were then used for nanofluid application. It was found that 600 rpm of the planetary ball-mill yielded larger particle size GFs (757.5 nm) than at 200 rpm (328 nm). The authors attributed this occurrence to the weight of the zirconia balls and excessive centrifugal forces that eventually disrupted the collision interactions between the metal balls and the starting material. GFs of smaller size show a higher surface area and they are more efficient in heat transfer. Besides, low speed ball-milling can minimize intense shock stress that can damage the graphite in-plane crystal; the shear stress is the dominant

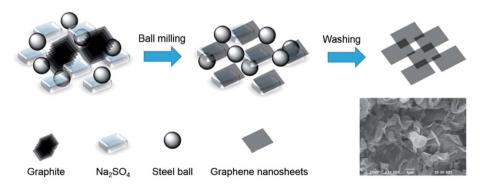


Fig. 1 Schematic of the soluble salt-assisted (Na_2SO_4) wet ball-mill route for the synthesis of graphene nanosheet powder. The inset is the SEM image of the produced GFs. Reprinted with permission from ref. 49.

Table 2 Examples of GF synthesis via wet milling and their characteristics

Equipment, ball type, ball size	Surfactant/solvent	Speed, duration	Graphene characteristics	Remarks	References
Ceramic grinding chamber, yttria zirconia ball, 50 & 100 µm	Sodium dodecyl sulfate (SDS)	233–2100 rpm, 3 hours	Mono- and multilayer, 25 g ${ m L}^{-1}$ produced, $I_{ m D}/I_{ m G}=\sim\!0.6$		82
Zirconia ball, 2 mm	SDS	100 rpm, 12 hours	Monolayer and few-layer, $I_{ m D}/I_{ m G} < 0.05$	Wet-milling was subsequently followed by sonication for 2 hours with 80 W power output	41
Milling container	N-methylpyrrolidone (NMP)	500 rpm, 10 hours	Multilayer, production rate = 0.0085 mg mL ⁻¹ h ⁻¹ , $I_D/I_G = \sim 0.24$	Wet milling in <i>N</i> -methylpyrrolidone	87
Planetary ball-mill, zirconia ball, 1 mm	Distilled water	200 rpm, 1 hour	GF particle size = 328 nm, λ = 680 mW m ⁻¹ K ⁻¹	The GFs produced were used in nanofluids based on distilled water	88
	<i>N,N</i> - Dimethylformamide (DMF)	300 rpm, 30 hours	Single- and few-layer GF <4 layers, $I_{\rm D}/I_{\rm G} = \sim 0.34$	DMF was a toxic solvent with a high boiling point of 153 °C	89
Tungsten carbide jar	Methanol	300 rpm, 30 hours	Few layer graphene, $I_D/I_G = 0.37-0.38$, electrical conductivity = 6700 S m ⁻¹	1-Pyrenecarboxylic acid $(C_{17}H_{10}O_2)$ was used as an exfoliant	86
Stainless steel pot, stainless steel ball, 5 mm		500 rpm, 12 hours	Chemically functional trilayer and few layer graphene, $I_{\rm D}/I_{\rm G}=0.025$ (after heat treatment)	Oxalic acid $(C_2H_2O_4)$ was used as a milling agent	85

force in the process. The exfoliation and fracture of the graphite particles were generally caused by shear and compression forces generated from the motion of the balls. Compression forces are predominant at the beginning as the size of graphite is large whereas the shear force can cleave graphite from their outer surfaces as the lateral size of the GFs gets smaller and the van der Waals forces weaken. It is important to avoid excessive compression forces so as not to damage the crystallinity of graphene. To minimize damage on the GFs, a shear-force dominated mechanism needs to be ensured and this is the reason why a low milling speed was practiced. This, however, increases the processing time.

In contrast to dry milling, wet milling does not require the presence of protecting gas to minimize GF oxidation but demands an additional purification step to remove the used exfoliants and solvents after the completion of the milling process. Occasionally, due to intensive reactions between the solution and the graphitic materials along with the milling forces, it can cause further contamination to the resulting graphene. It seems that both routes have their pros and cons but in terms of scale, quality and volume of produced GFs, dry milling does tick all the boxes. Overall, the ball-milling technique has some advantages: production of high quality GFs, it is highly scalable and the size of GFs can be varied by a simple modification of the milling parameters, but most often this method involves long processing cycles that reduce the yield rate of GF production.

2.2 Explosion and shockwaves

In the past, fullerene and carbon nanotubes were obtained by exploding graphite, iron and nickel wires in organic

solvents.90-92 Unlike other methods, explosion-driven GF synthesis has a very short lead time. The explosion provided sufficient energy injection to exfoliate graphite, which then reacted with metal catalysts. However, it is a very delicate process whereby excessive energy injection would damage the graphene crystallinity, and similar effects were observed in the case of excessive compression force in ball-milling of graphite.87

Graphene synthesis via detonation was first discovered by Nepal et al. 93 who produced gram scale graphene nanosheets via controlled detonation of acetylene (C₂H₂) in the presence of O₂. The experimental setup being utilized was the same for normal carbonaceous soot synthesis. However, the peak detonation temperature was roughly twice (4000 K) the combustion temperature for soot production. As a result, most hydrogen was removed from the main chamber leaving just pure carbon with graphene-like characteristics. The presence of GFs after detonation-driven synthesis was verified by Raman spectroscopy and it was found that the best structural quality of GFs can be obtained at high O₂ to C₂H₂ ratios. The authors suggested that during the detonation, which only lasted about 15 ms, the hydrocarbon was first converted into free carbon atoms and ions. The chamber was then allowed to cool to 300 K at which the carbon atoms and ions condensed into carbon nanoparticles that quickly aggregated into GFs. Most of the hydrogen from acetylene was removed from the chamber together with oxygen. Otherwise, carbonaceous soot has been found within the chamber.

Gao et al. 94 managed to produce mono- and few-layer GFs via explosion generated by electric wire explosion charge voltage on high-purity graphite sticks in distilled water at ambient temperature. During this short burst of energy carried by the explosion, the graphite was exfoliated and broken into smaller pieces of GFs. The schematic diagram in Fig. 2 illustrates the mechanism of the explosion process for graphene synthesis. The energy injection or explosion needs to be powerful enough to overcome the van der Waals forces but not too powerful that it could completely disrupt the fundamental crystallinity of graphene. In this case, less than 10 layers of graphene can be obtained within the charging voltage of 21–25 kV and the optimal value to get monolayer graphene was found to be around 22.5 to 23.5 kV.

Meanwhile, Yin *et al.*⁹⁵ took a different approach. They synthesized GFs *via* a one-step shockwave-driven treatment. Instead of just breaking graphite into smaller pieces of GFs, herein, three compounds in the form of calcium carbonate (CaCO₃), magnesium (Mg) and ammonium nitrate (NH₄NO₃) were used concurrently as the carbon source, reductant and nitrogen-doping source, respectively. Nitromethane (CH₃NO₂)

was used as the main charge to thrust the steel flyer to a high velocity (1 to 3 km s⁻¹) within the stainless steel sample container. The subsequent explosion initiated extremely rapid shock-induced decomposition and chemical reaction that converted carbonate into multilayer graphene and nitrogen-doped graphene as shown in eqn (1) to (3) and Fig. 3. The same template was then used to synthesize few-layer graphene (FLG) sheets from dry ice (solid CO₂) with calcium hydride (CaH₂) and NH₄NO₃.96 In this work, an electronic detonator was utilized with the main charge being cyclotrimethylenetrinitramine or RDX (C₃H₆N₆O₆), which initiated the shockwave. The whole operation per process cycle was tightly controlled to be completed within 90 s. The shockwave explosion normally lasted for a very short duration of around 10⁻⁶ s. The rest of the lead time was to give time for the recovered container to settle down before it is safe to be opened to remove the sample.

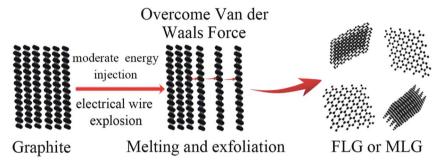


Fig. 2 Illustration of the proposed mechanism for the formation of graphene nanosheets in electrical explosion of graphite sticks. Reprinted with permission from ref. 94.

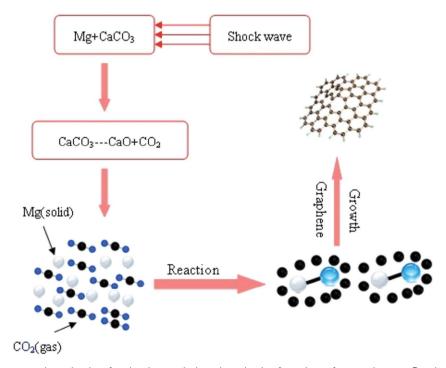


Fig. 3 Illustration of the proposed mechanism for shockwave-induced synthesis of graphene from carbonate. Reprinted with permission from ref. 95.

$$CaCO_3 \rightarrow CO_2 + CaO$$
 (1)

$$2Mg + CO_2 \rightarrow C' + 2MgO$$
 (2)

$$C' \rightarrow graphene$$
 (3)

Table 3 compiles the studies related to explosion and shockwave exfoliation that have been described earlier. The main advantage of these methods is the significantly short processing time and thus they produce GFs at a high yield rate. However, they are quite dangerous and require strict safety precautions when executing experimental studies. This is probably the reason why the number of research groups undertaking these methods for GF synthesis is considerably low but more studies would be possible if a clear standard consideration of safety and the detailed procedure in the operation process involved are available. These methods generally operate in a very delicate manner and they require precise control of the reaction conditions since the system is quite sensitive to even a small change in processing parameters that can have an enormous effect on the quality of GFs produced. This attested to the complexity of the process, which may be due to its infancy for GF synthesis, but it might be the answer to the mass-production of GFs in the future. More studies are needed to be done in a more systematic approach to refine the current explosiondriven methods by optimizing the reaction conditions for GF synthesis.

2.3 Sonication

Sonication is a potent tool for extracting nanomaterials from the bulk starting material97,98 and it was also widely used to suppress the aggregation of carbon nanomaterials in solvents. Before graphene became prevalent, there were a number of groups that had studied exfoliation of CNTs in solvents.99 One of them, Bergin et al.100 found that solvents with surface energy close to that of CNTs would be a good medium to disperse them. Graphite has a surface energy comparable to that of CNTs, and hence, the exfoliation of graphite to graphene in certain solvents that had been used for CNTs would be possible. When solvents with surface energies close to that of graphene are used (i.e. around 68 mJ m⁻²),101 the mixing enthalpy is minimized, which favors the graphite exfoliation process.

Khan et al. 102 demonstrated the preparation of GFs in NMP at a concentration up to 1.2 mg mL^{-1} via an extended bath sonication for up to 460 h or \sim 19 days. NMP is a good solvent for exfoliation of graphite via sonication, but unfortunately, its high boiling temperature of 202 °C forbids its easy removal. 103 GFs dispersed in high boiling point solvents have been transferred to a low boiling point solvent via solvent exchange 104 but the obvious solution would be direct exfoliation of graphite to graphene in a low boiling point solvent that can also provide a more stable dispersion. O'Neill et al.105 demonstrated this by exfoliating graphite via a low power sonication bath in chloroform (CHCl₃; boiling point = $61.2 \, ^{\circ}$ C), isopropanol (C₃H₇OH; boiling point = 82.6 °C) and acetone (C_3H_6O ; boiling point = 56.0 °C).

At this point, it is obvious that many research groups have used NMP as a solvent for sonication assisted graphene exfoliation. This is due to the fact that the surface energy of NMP well matches with that of graphene, favoring exfoliation to occur freely.103 However, NMP does not only possess a high boiling point but it is also relatively expensive. Water can be a good alternative but unfortunately, it has a very high surface energy to

Table 3 Examples of GF synthesis via explosion and shock-waves and the characteristics of produced graphene

Explosion or shock-wave conditions					
Equipment, main charge	Carbon source, reductant, nitrogen source	Explosion conditions	Characteristics of produced graphene	Remarks	References
Cylindrical aluminium chamber	Acetylene (C ₂ H ₂)	Peak detonation temp. $= 4000 \text{ K}$, peak detonation pressure $= \sim 13.3 \text{ atm}$, $t_{\text{Detonation}} = \sim 15 \text{ ms}$	Mono- to tri-layers, size = $35-250$ nm, $I_{\rm D}/I_{\rm G} = \sim 0.28-1.33$, specific surface area = $23-187$ m ² g ⁻¹	Detonator = spark generator ignition system, production rate = $300 \mathrm{g}\mathrm{h}^{-1}$	93
Cylindrical stainless steel explosion chamber	Graphite stick	Optimal charging voltage = 22.5–23.5 kV	Mono- and few-layer, $I_{\rm 2D}/I_{\rm G}$ = 1.83–2.09, $I_{\rm D}/I_{\rm G}$ = 0.06–0.12	Complex purification step with 4.4 M 15% HCl being used	94
Stainless steel sample container, nitromethane (CH_3NO_2)	Calcium carbonate, magnesium, ammonium nitrate	Impact velocity = 3.37 km s ⁻¹ , shock pressure = 22.1 GPa, shock temp. = 5215 K	Multilayer and nitrogendoped, $I_{\rm 2D}/I_{\rm G}=1.43$, $I_{\rm D}/I_{\rm G}=0.6$, FWHM $_{\rm 2D}=41$	For purification, nitric acid was used under heating conditions. Then, the sample needs to be filtered and freeze dried	95
RDX $(C_3H_6N_6O_6)$	Dry ice (solid CO ₂), calcium hydride (CaH ₂), ammonium nitrate	Impact velocity = 3.37 km s ⁻¹ , shock pressure = 22.1 GPa, shock temp. = 5215 K	Nitrogen doped few layer and few layer, $I_{ m 2D}/I_{ m G}=1.63,$ $I_{ m D}/I_{ m G}=0.89$	Diluted hydrochloric acid was used for purification. RDX is a more energetic explosive than trinitrotoluene (TNT) which is quite dangerous	96

be used as an exfoliant for graphene. Not to mention, graphene is hydrophobic in nature. With these factors in mind, Lotya $et~al.^{106}$ dispersed graphite in surfactant–water solutions, with sodium dodecylbenzene sulfonate (SDBS) as the surfactant, in a low power sonic bath for 30 min. The exfoliated GFs and graphitic flakes were stabilized against re-aggregation by Coulomb repulsion due to the adsorbed surfactants. It would take around 6 weeks for the larger flakes to sediment. Other types of surfactants such as bile salt sodium cholate $(C_{24}H_{41}NaO_6),^{107}$ 7,7,8,8-tetracyanoquinodimethane (TCNQ; $C_{12}H_4N_4)^{108}$ and cetyltrimethylammonium bromide (CTAB; $C_{19}H_{42}BrN)^{109}$ have also been investigated.

Sonication-driven graphene synthesis can be done either by using bath-sonication or tip-sonication. Bath-sonication is cheaper but has a serious reproducibility issue. The sonic energy emitted to the sample in bath-sonication can vary depending on the water level, volume of dispersion, vessel shape, power output and exact position of the sample. It also tends to take a longer processing time, which can lead to water evaporation. To enhance the performance of bath-sonication, a pressurized ultrasonic bath reactor can be used to intensify the generated ultrasound. For instance, Štengl¹¹⁰ synthesized non-oxidized GFs from powdered natural graphite *via* high-intensity cavitation fields in a pressurized (5 bar) ultrasonic

reactor. The cavitation fields that involve the oscillations and collapse of cavities (bubbles) in the liquid provided the source of energy to enhance a wide range of chemical processes and provide physical effects to break down the graphite into GFs.¹¹¹

Table 4 compiles all the work related to the aforementioned sonication-driven processes for GF synthesis. In summary, the exfoliation of graphite via the sonication route is heavily dependent on the type of solvent and surfactant being used to contain the graphite. It can be concluded that it is essential for the medium to have the required surface energy that matches well with that of graphite, thus favoring the exfoliation process to occur. Since the surface energy of graphene is close to that of CNTs, the type of suitable solvent and surfactant can be easily determined because there have been a wide range of studies conducted on these materials for CNT dispersion in the last two decades. This, among others, fosters the fast advancement of this technique. Another advantage of solvent-based techniques for GF synthesis is the readiness of the solution post-exfoliation process to be immediately used for various solution-based applications such as nanofluids, spray painting, spin coating, etc. The yield of GFs from the sonication-driven exfoliation process is considerably low but improvement can be achieved by prolonging the sonication time but at the expense of the quality of the produced GFs. In most cases, this technique

Table 4 Examples of GF synthesis via sonication and their characteristics

Sonication conditions				
Equipment	Starting material, solvent/ surfactant	Sonication time, sonication power	Graphene quality	References
High pressure ultrasound reactor (HPUS), pressure = 5 bar	Graphite ore, dichloromethane (CH ₂ Cl ₂) or octanol C ₈ H ₁₇ OH	10, 30, 50 minutes, 1.3 kW	Few layer, size = \sim 380–1100 nm	113
Sonication was preceded by pressing and homogenization	Carbon nanotubes, NMP	15 minutes	GFs, size = \sim 40–50 nm, $I_{\rm D}/I_{\rm G}$ = 1.02–1.30	114
Low power sonic bath	SDS	30 minutes	Monolayer (\sim 3%), multilayer ($<$ 5 layers), $I_{\rm D}/I_{\rm G}=0.4$	106
Pressurized ultrasound reactor, pressure = 5 bar, flow rate = 10 mL min^{-1}	Natural graphite, aqueous ethylene glycol $(C_2H_6O_2)$	50 minutes, 1 kW	Non-oxidized GFs, $I_{\rm D}/I_{\rm G} = \sim 1.2$	110
Bath sonicator	Natural graphite, NMP	∼460 hours, 23 W	Multilayer graphene (<10 layers), graphene concentration = \sim 1.2 mg mL ⁻¹ , mean flake length = >1 μ m, $I_D/I_G = 0.3$ –0.6	102
Low power sonic bath	Natural graphite, chloroform $(CHCl_3)$ or isopropanol (C_3H_7OH)	48 hours, ∼16 W	Multilayer graphene, <10 layers for chloroform, <6 layers for isopropanol, length = \sim 1 μ m, $I_{\rm D}/I_{\rm G} = \sim$ 0.35 to \sim 0.55 (for 22–70 h sonication)	105
	Natural graphite flakes, aqueous sodium cholate		Graphene conc. = 90 μg mL ⁻¹ , $I_{\rm 2D}/I_{\rm G} = 0.8$ -2.1, $I_{\rm D}/I_{\rm G} = \sim 0.93$	107
	Commercial expanded graphite, 7,7,8,8- tetracyanoquinodimethane $(C_{12}H_4N_4)$ anion	90 minutes	Single or few-layer, 2–3 layers, graphene conc. = \sim 15–20 μg mL ⁻¹ , thickness = 2.36–2.97 nm	108
	Highly ordered pyrolytic graphite (HOPG), cetyltrimethylammonium bromide $(C_{19}H_{42}BrN)$	4 h	FLG, thickness = \sim 1.18 nm	109

would produce GFs with relatively inferior quality than the other techniques due to scission, which is a known effect induced by sonication that can destroy the graphene sheets and can cause a drastic drop of lateral dimensions of GFs. 80,112 Besides, the scalability of this technique is hampered by the utilization of ultrasound as the energy source.

Electrochemical exfoliation

In the past, electrochemical exfoliation has been employed on graphite oxide in electrolyte solutions such as sodium sulfate115 and phosphate buffer saline (PBS; K2HPO4/KH2PO4).43 Nonetheless, the formed sp³ defects cannot be efficiently transformed to sp² because graphite oxide was used as the starting material. Recent developments of using graphite as the starting material in electrochemical exfoliation were able to increase the quality and quantity of the produced GFs.

A quintessential experimental setup for electrochemical exfoliation would normally involve a working electrode and a counter electrode connected to a power source immersed in an electrolyte. The working electrode is the subject of the process and most often it is in the form of rods or foil made up of the graphitic material. The applied potential is the critical force in driving the reaction between the electrolyte and the electrodes leading to the exfoliation of graphite. Either anodic or cathodic potentials are able to drive ions typically from the electrolyte into the graphitic inter-layers, and these ions then promote structural deformation of graphite and break down into graphene.

The control of electrode potential is vital in altering the thickness and surface properties of exfoliated graphene. Morales et al.116 found that graphene with different degrees of oxidation were obtained by controlling the electrochemical potential. In order to achieve higher precision in controlling the applied potential, a two-electrode system was deemed inadequate. In this regard, a three-electrode system was proposed. Aside from the working electrode and a counter electrode, a three-electrode cell setup has an additional reference electrode. If the working electrode operates as a cathode, then the counter electrode will function as an anode and vice versa. Electrochemically inert materials such as platinum or carbon are normally used as the counter electrodes in graphene exfoliation.117 This is done to avoid any unwanted reaction from happening on the counter electrode that would taint the produced GF. The counter electrode is there to complete the circuit for current to flow along with the working electrode and the solution medium. On the other hand, the reference electrode does not take part in the electrochemical exfoliation.116 There is little to no current flowing through the reference electrode. The reference electrode commonly functions as a reference to the working electrode without compromising the stability of the process. Alanyalioğlu et al. 117 investigated the use of a three-electrode system in SDS solution where the graphite rod, Pt foil and Pt wire function as the working electrode, counter electrode and quasi-reference electrode, respectively. The electrochemical process was divided into two steps. The first step involved the electrochemical intercalation of SDS into graphite which was then followed by

electrochemical exfoliation of the SDS-intercalated graphite electrode as shown in Fig. 4. By increasing the intercalation potential, the cyclic voltammograms shift to a positive potential, which was attributed to the increase of size or concentration of GFs in the suspensions. Furthermore, the presence of SDS surfactant prevents the GFs from re-stacking in the solution and yields a stable graphene suspension.

The commonly used graphite rod or foil possesses a rather limited surface area and only the outer part is exposed to the electrolyte solution for exfoliation. A graphitic material in the form of powder or porous scaffold would offer a significantly larger surface area, thus enhancing the efficiency of the exfoliation process resulting in yield improvement. Sharief et al. 118 explored this avenue by binding carbon black particles together with an electrically conductive polyaniline binder to form a porous electrode with higher surface area than the conventional graphite rod and foil. FLG was obtained from this process. In an earlier study, Alfè et al. 119 also synthesized GFs from strongly oxidized carbon black particles that require a multi-step chemical route involving harsh chemicals such as hydrazine hydrate (N2H4). Besides, the yield of GF production can also be enhanced by using an acidic electrolyte but it can cause over-oxidation of graphite. This is the reason why an electrolyte system using aqueous inorganic salts at neutral pH was used in the work by Parvez et al. 120 and they showed a good balance between the quality and quantity of the produced GFs.

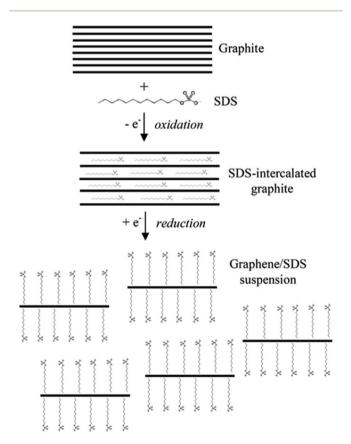


Fig. 4 Schematic illustration of the proposed electrochemical exfoliation route to produce a graphene/SDS suspension. Reprinted with permission from ref. 117.

As indicated earlier, electrochemical exfoliation can be performed under anodic and cathodic potentials. The former promote anions of the electrolyte to intercalate into the layerstructured anode due to the electrical field. Simultaneously, it will also intensify the splitting of water into hydroxyl radicals which are highly oxidative mainly towards the graphite electrode.121 Anodic exfoliation usually involves the use of aqueous electrolytes such as sulfuric acid, sodium benzoate, sodium citrate and triethyl-methylammonium-methylsulfate (TEMAMS), 122,123 resulting in the generation of HO* radicals from water electrolysis which can disrupt the graphitic structure. Yang et al. 121 carried out electrochemical exfoliation in the presence of antioxidants with the intention of suppressing the formation of radicals. TEMPO (2,2,6,6-tetramethylpiperidin-1yl)oxyl) assisted electrochemical exfoliation was used to produce large graphene nanosheets with an extremely high carbon to oxygen ratio (\sim 25.3). Meanwhile, the generation of oxygenated functional groups is minimal in cathodic exfoliation because it employs an organic electrolyte, which is non-oxidizing, in contrast to the aqueous solution used in anodic exfoliation. Therefore, cathodic exfoliation is preferred to minimize the formation of graphite oxide but anodic intercalation is more efficient in terms of the duration of the exfoliation process.116 Depending on the pH, type and concentration of electrolyte used, the commonly applied potential in anodic exfoliation is +10 V or below. 44,112,114,117 However, cathodic exfoliation would require a substantially greater potential (up to -30 V in one case)124 to produce graphene since a lower cathodic potential would lead to an inefficient and slower exfoliation process. 125 This is the reason why a cathodic route normally relies on the subsequent process such as sonication in order to complete the exfoliation process if a lower applied potential is used. 116,126

Regarding the mechanism of the electrochemical exfoliation method, it depends on the type of applied potential utilized towards the working electrode127 that determines whether it is cathodic or anodic. In cathodic exfoliation, negative current supplies electrons to graphite, creating a negatively charged graphite. The negative charge condition promotes positive charge ions to intercalate between the interlayer spacing of graphene. 128,129 The same is true for the opposite. Positive current withdraws electrons from graphite, creating a positively charged graphite, which promotes intercalation of negative ions between the interlayer spacing of graphene. Exfoliation of graphite occurs as the intercalation or insertion of ions into the interlayer spacing of graphene opening up the van der Waals gap between the graphene layers and subsequent expansion would eventually cause separation from one another. In some cases, the intercalant or cointercalant species evolve into gases, which then assist the exfoliation of the graphite layers. For example, Parvez et al. 120 used aqueous (NH₄)₂SO₄ solution in a 2-electrode cell anodic exfoliation setup. When enough energy was supplied to the process, oxygen and carbon dioxide gases were produced which aided the exfoliation of graphite layers. In another study, the Li⁺/propylene carbonate electrolyte was used and propylene gas was detected from the decomposition of the organic solvent on the cathode. 126

In general, electrochemical exfoliation was normally chosen to synthesize GFs because it is facile, economic, environmentally

friendly, non-destructive and operates at ambient pressure and temperature. Furthermore, it is a versatile technique in a way that the characteristics of the produced GFs can be controlled easily, for instance the GF thickness can be modulated by merely adjusting the electrode potential. Besides, a high yield rate of GFs can be achieved using this technique due to its relatively short processing time. For mass production, anodic exfoliation is more preferable than cathodic exfoliation, but oxidation of GFs needs to be minimized in order to meet the structural quality required for application. Table 5 summarizes the studies previously described in the electrochemical exfoliation of graphite for GF synthesis.

2.5 Shear exfoliation in liquid

Sonication-based exfoliation generally operates in an ultrasonic water bath or via probe-tip sonicator which has limited scalability. Sonic tips and sonic baths can only be effective when processing volumes no larger than a few hundred milliliters. 102,103,133,134 The energy transfer from the energy source to the liquid medium is relatively poor leading to low production rates. Expanding the volume of the liquid medium in a sonication-based exfoliation would weaken the sonication energy. At manufacturing scale, sonication of graphite to graphene does not seem to be a viable method. Plus, it was reported that sonication-based exfoliation has a sublinear increase in GF concentration (C_{GF}) with sonication time (t), represented by C_{GF} $\propto \sqrt{t}$ which means that the sonication time has a significantly lower impact at higher concentration. 102,134 Recent studies demonstrated that shear mixing of graphite in aqueous surfactants or solvents could lead to efficient exfoliation to FLG135,136 as a scalable alternative to sonication-based exfoliation. For shear-based exfoliation, GF concentration typically scaled as $C_{\text{GF}} \propto t$ in surfactant solutions. 136

In the past, shear mixing was extensively used to disperse and scatter nanoparticles in liquid media by breaking up the weakly bound nanoparticle agglomerates137 but it can also be employed to disrupt the stronger van der Waals forces in the graphite layers to produce graphene at a lower energy density than that of the ultrasonic probe. 136,138 A typical shear-based exfoliation would involve the use of a rotating blade or rotor in a solvent, surfactant or aqueous medium mixed with graphite. It is also critical that shear-exfoliation can be done without any pre-treatment such as intercalation so that the potential to scale the technology is not limited by the intercalation step. For example, the additional "wireless" electrochemical intercalation of graphite flakes prior to high-shear exfoliation in the work by Bjerglund et al. 139 was seen as a stumbling block for commercialization although a remarkable GF yield of around 16% was obtained.

In the early days of shear exfoliation of graphite in liquid, Chen et al. 138 utilized shearing vortex fluidic films in a rapidly rotating tube (7000 rpm) inclined at 45° as shown in Fig. 5. The degree of the inclination plays a vital role as the shearing stress arises from interactions between centrifugal and gravitational forces. Slippage of graphene also occurs on the walls of the tube as the graphite bulk material was held against the tube walls by

Table 5 Examples of GF synthesis via electrochemical exfoliation and their characteristics

Applied potential, remarks	Configuration, working electrode, counter electrode, quasi-ref. electrode	Electrolyte, duration	Characteristics of produced Graphene	References
3 V	2-Electrode cell, high purity graphite rods, Pt sheet	NaOH/H ₂ O ₂ /H ₂ O, 10 min	Anodic few-layer, 3 to 6 layers, yield = 95%, $I_D/I_G = 0.67$	44
2 V	3-Electrode cell, graphite rod, Pt foil, Pt wire	SDS (0.1 M)	Multi-layered GFs, size _{Average} = \sim 500 nm, thickness = \sim 1 nm, $I_D/I_G = 0.124$	117
-1.0 V, sonication-assisted exfoliation	3-Electrode cell, 1 mm thick graphite foil, large surface area carbon, normal hydrogen electrode	Aqueous perchloric acid	Few layer, 3–6 layers, $I_{\rm D}/I_{\rm G}=0.478$	116
1, 3, 5 V	2-Electrode cell, carbon black particles bind with polyaniline into a porous electrode, Pt wire	5 min, 4 h, 3 h	Few-layer, length = \sim 35 nm, width = \sim 30 nm, thickness = 3-8 nm, $I_D/I_G = \sim$ 0.875	118
${\sim}2~V~\mu m^{-1}$	3-electrode cell, carbon nanofiber grown on stainless steel, Pt mesh, Ag/AgCl	Sulfuric acid solution (0.5 M)	Graphene/CNF hybrid, $\beta = 4930$, turn-on voltage = 1.34 V μ m ⁻¹	130
10 V	2-Electrode cell, graphite flake, Pt	Aqueous sulfate salt, 3–5 min	Yield =>85% (3 layers), lateral size = 44 μ m, C : O ratio = 17.2, hole mobility = 310 cm ² V ⁻¹ , $I_D/I_G = 0.25$	120
1–10 V, shear-assisted electrochemical exfoliation	2-Electrode cell, HOPG, Pt	Sulfuric acid (0.1 M), 43 s	GFs, size = \sim 10 μ m, $I_{\rm D}/I_{\rm G}$ = 0.21–0.32	131
2.977 V, sonication-assisted electrochemical exfoliation	3-Electrode cell, graphite plate, Pt, Ag/AgCl (3 M KOH)	Electrolyte = SDS	Graphene nanosheets, in- plane crystallite size $(L_a) = 26.8$ nm	132
+3 V	2-Electrode cell, pre-treated graphite foil, Pt	30 min	Graphene nanosheets, lateral size = $<2 \mu m$, $I_D/I_G = 0.60$	123
	2-Electrode cell, rolled graphite foils, Pt foils	ТЕМРО	Graphene nanosheets, size = 5–10 μ m, $I_{\rm D}/I_{\rm G}$ = <0.1, C/O = \sim 25.3	
-15 ± 5 V, sonication-assisted exfoliation	Graphite in liquid- rechargeable lithium ion batteries	Propylene carbonate	Few-layer, <5 layers, yield = >70%	126
−15 to −30V	2-Electrode cell, HOPG rod, Pt- sheet	<i>N</i> -Butyl,methylpyrrolidinium bis(trifluoromethylsulfonyl) imide (BMPTF ₂ N)	2–5 layers graphene sheets, low levels of oxygen (2.7 at% of O), $I_{\rm D}/I_{\rm G} < 0.05$	124

centrifugal forces. Without the inclination, there would be no exfoliation as centrifugal forces would be the lone force present, which resulted in less turbulence within the liquid medium. Unfortunately, this method is considered a 'soft energy' source whereby the shear stress is quite limited for the exfoliation process, thus resulting in a low GF yield (~1 wt%). In order to achieve a higher yield, the level of shear stress needs to be raised. One way to elevate the shear stress is by incorporating the fluid dynamics phenomena in the exfoliation process such as turbulence-induced shear stress.140

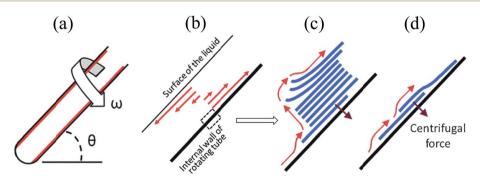


Fig. 5 (a) Schematic illustration of the exfoliation process using a vortex fluidic device inclined at 45°; (b) micro-fluidic flow velocity of the rotating tube; (c) exfoliation process from centrifugal and gravitational forces; (d) slippage of the graphene layer on the inner surface of the tube. Adapted with permission from ref. 138.

Paton et al. 136 worked on high-shear mixing of graphite in sodium cholate (NaC) and NMP via a rotor-stator system which resulted in large-scale exfoliation of un-oxidized graphene nanosheets. The rotor-stator system provided higher shear stress for the exfoliation phenomenon. A model was also developed showing that exfoliation occurs once the local minimum shear rate exceeds 10⁴ s⁻¹. The experimentations were carried out initially in a 5 L high-shear mixer (rotor diameter = 3.2 cm) and later expanded into a 300 L high-shear mixer (rotor diameter = 11 cm). The large-scale trials yielded 21 g of GFs per batch with low I_D/I_G and production rates as high as 5.3 g h⁻¹. Both followed the same scaling law and it was estimated that production rates of 100 g h⁻¹ are possible at 10 m³ volume. Additionally, the need for turbulent energy for exfoliation was also proven to be unnecessary as exfoliation can still happen even when turbulence did not fully develop at a Reynolds number (Re) less than 10 000. This means that as long as the mixer can achieve this minimum shear rate, it can be used to produce GFs, regardless of whether turbulence is achieved or not. However, it is important to note that a higher Re number represents higher shear stress and hence GF production at higher yield compared to that produced in laminar flow can be expected. In a study by Varrla et al., 135 a Kenwood kitchen blender was employed to produce graphene. Graphene was able to be synthesized because the mean turbulent shear stress within the kitchen blender exceeds the critical shear rate for the exfoliation of graphite. From this study, it appeared that the use of an industrial rotating blade continuous stirred tank reactor (CSTR) can be an upgrade for a large-scale production of GFs.

Tran et al.141 showed that high shear mixing of graphite powders in NMP with the implementation of the Taylor vortex flow regime resulted in an efficient exfoliation into FLGs with a high yield. This secondary flow ensued when the rotation of the inner cylinder between two concentric cylinders exceeds a critical value with the outer cylinder fixed as shown in Fig. 6. The critical value for Taylor vortex flow can be identified using the Taylor number (Ta) as illustrated in eqn (4). Ω is the angular velocity, R_i is the radius of the inner cylinders, R_0 is the radius of outer cylinders and ν is the kinematic velocity. Taylor instability

sets in when Ta exceeds ~1700 as highly turbulent Taylor vortex flow is developed prompting a high wall shear stress and pressure sufficient to produce a high yield of GFs. Besides, shear exfoliation is quite flexible and can be combined with other techniques to improve the overall performance of the process.

$$Ta = \frac{Q^2 R_i (R_o - R_i)^3}{v^2}$$
 (4)

Table 6 summarizes the studies previously described in the shear exfoliation of graphite in liquid for GF synthesis. Generally, this technique shares the same advantages as the sonication-driven exfoliation technique such as a wide selection range of solvents and surfactants, and the readiness for immediate utilization for solution-based applications. However, in the aspect of yield production and quality of synthesized GFs, the shear exfoliation technique is superior to that based on sonication. In fact, this technique has demonstrated the highest production rate (5.3 g h⁻¹) of high quality GFs¹³⁶ compared to the other techniques, which offers great potential for scale-up and mass production.

3 **Future prospects**

The safety aspect is the top consideration when comes to any kind of production process. From the methods presented in this review, explosion-based exfoliation would be the most dangerous since it involves the use of explosive materials. These materials would need special care and safety precautions while also demanding lengthy and complex procedures for purchasing them. This is different than the flammable gases widely used in the CVD process since the threat of them being dangerous to the operators has been exhaustively investigated and the standard operating procedures in handling them have long been established. There are also too many unknown variables to provide the necessary external energy to breakdown graphite in explosion-based exfoliation. Even a slight difference in the position and quantity of the explosives can bring about different quality of GFs.

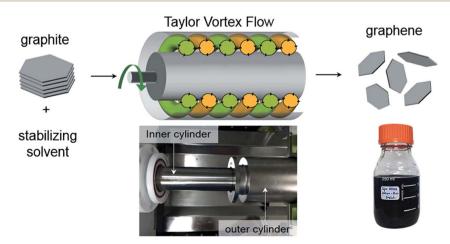


Fig. 6 Schematic illustration of GF synthesis via shear-based exfoliation using Taylor vortex flow. Reprinted with permission from ref. 141.

Table 6 Examples of GF synthesis via shearing-based exfoliation and their characteristics

Shearing conditions				
Equipment, remarks	Solvent/surfactant	Duration, speed	Graphene quality	References
Silverson model L5M mixer, rotor diameter = 32 mm, liquid volume = 4.5 L	NMP and NaC (sodium cholate)	20 min, 4500 rpm	FLG nanosheets, size = 300–800 nm, thickness _{ave} = 4–7, $I_{\rm D}/I_{\rm G}$ = 0.17–0.37	136
High-shear mixer, rotor diameter = 110 mm, liquid volume = 300 L		5 min to 4 hours, 3000 rpm	Production rate = 5.3 g h $^{-1}$, conc. = 0.07 mg mL $^{-1}$, $I_{\rm D}/I_{\rm G}$ = 0.18	136
Two co-axial cylinders Taylor– Couette flow reactor	NMP	60 min, 3000 rpm	Few-layer GFs, lateral size = 500–1500 nm, thickness = <3 nm, $I_{\rm D}/I_{\rm G} = \sim 0.14$, yield = 5%	141
Kenwood BL370 series kitchen blender, working volume = 500 L, motor = 400 W	Fairy washing-up liquid (FL)	5–30 min, 18 000 rpm	Lateral size = hundreds of nm, max flake length = \sim 3.3 μ m, $I_{\rm D}/I_{\rm G} = 0.3$ –0.7, FWHM = \sim 45 cm ⁻¹	135
Vortex fluidic device, tube inclination = 45°	NMP	30 min, 7000 rpm	Few layer GFs, yield = \sim < 1 wt%, max size = 1 μ m, thickness = \sim 1 nm	138
Pro Scientific PRO250 rotor- stator, shear rate = $33\ 000\ s^{-1}$		1 h, 6000 rpm	Size = 0.4–1.5 μ m, thickness = 4–6 layers, yield = 16%, $I_{\rm D}/I_{\rm G} = \sim 0.24$	139
High-speed steel blender, blade diameter = 28 mm	Aqueous modified polyvinyl alcohol (mPVOH)	24 000 rpm	Size = \sim 400 nm, thickness = 5-10 layers	142

This leaves us with electrochemical, sonication, ball milling and shear exfoliation in liquid. Among others, the potential to scale-up the process would be the most vital aspect in comparing them. Based on the detailed description for each method given in this review, it appeared that the limited processing volume for sonication and electrochemical-based exfoliation restricts their scalability. In contrast, to scale-up shear in liquid and via ball milling is rather easy and this is logical since they have been in the commercial sector for a very long time. There are various CSTRs and ball-mills available in the market that can be used to replicate and scale-up the laboratory-scale process. Between these two methods, shear exfoliation in liquid offers greater advantage due to simpler operation, since the presence of inert gas in the case of dry milling and the requirement for an additional purification step in wet milling makes the milling process rather complicated. Furthermore, ball milling requires a longer processing cycle. Factoring these aspects into the equation, shear exfoliation in liquid offers the brightest prospect toward large-scale and low-cost GF synthesis.

Scaling up GF production from the laboratory-scale presents a huge challenge. It is a hurdle that needs to be overcome if a future where graphene is cheaply and easily mass-produced is ever to be achieved. There is no doubt that, with concentrated and cooperative efforts in research and development by the private and government sectors, GF production methods will quickly become more productive and cost-effective in the near future. In particular, for shear exfoliation in liquid, the critical aspect needed for scale-up is to have high shear rates and efficient processes, which can be achieved through a careful design of the flow regime which involves the aspect of flow dynamics. At the same time, the issue of process-induced defects and disparity in the size and number of layers of the produced GFs, which are common problems for all synthesis methods, should also be tackled.

Conclusion

In this review, we describe the synthesis methods of GFs by using ball milling, explosion, sonication, electrochemical and shear exfoliation in liquid. The mechanism of each method was described in the respective sub-sections. Results from the recent studies were compiled, presented and discussed. Finally, the methods were compared and their future prospects were expressed. After a comprehensive analysis of the GF synthesis methods presented in this review, shear exfoliation in liquid has emerged to be the brightest prospect for scaling-up GF production, not only because it is relatively safe, simple and cheap but also due to its technological maturity. Therefore, a coordinated effort in leading the research towards large scale and low cost production by focusing on shearing-based exfoliation is highly recommended to speed up the commercial availability of GFs and fulfil the surging demand for GFs in various technological applications to produce next-generation devices.

Conflicts of interest

There are no conflicts to declare.

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